

Catalytic hydrogen generator for use with methanolPatent Number: ☐ US4789540

Publication date: 1988-12-06

Inventor(s): JENKINS JOHN W (GB)

Applicant(s):: JOHNSON MATTHEY PLC (GB)

Requested Patent: ☐ EP0217532, B1Application
Number: US19860903644 19860904Priority Number
(s): GB19850021953 19850904

IPC Classification:

EC Classification: C01B3/32BEquivalents: AU580443, AU6215686, CA1290548, DE3666689D, ☐ ES2001647, JP2079113C,
☐ JP62059501, JP7098641B

Abstract

A catalytic hydrogen generator which generates hydrogen by the partial oxidation of methanol by oxygen (usually supplied as air) which comprises a gas permeable catalyst system having an upstream zone (2) filled with a copper catalyst supported on a refractory support (3) (for example silica or silicate granules) and a downstream zone (4) filled with a mixture of a similar supported copper catalyst and a platinum or palladium catalyst supported on a similar refractory support (5b). A mixture of methanol and oxygen is fed to the upstream zone and initially permeates through to the downstream zone where spontaneous oxidation of the methanol is initiated raising the temperature of the system to a level at which partial oxidation of methanol in the presence of the copper catalyst in the upstream zone (2) commences and produces hydrogen.

Data supplied from the esp@cenet database - I2

THIS PAGE BLANK (USPTO)



Europäisches Patentamt
European Patent Office
Office européen des brevets

Publication number:

**0 217 532
B1**

⑫

EUROPEAN PATENT SPECIFICATION

④⑤ Date of publication of the patent specification:
02.11.89

⑤① Int. Cl.⁴: **C01B 3/32**

②① Application number: **86306500.9**

②② Date of filing: **21.08.86**

⑤④ Catalytic hydrogen generator for use with methanol.

③⑦ Priority: **04.09.85 GB 8521953**

④③ Date of publication of application:
08.04.87 Bulletin 87/15

④⑤ Publication of the grant of the patent:
02.11.89 Bulletin 89/44

②④ Designated Contracting States:
AT BE CH DE FR GB IT LI LU NL SE

⑤⑥ References cited:
FR-A-2 490 615

⑦③ Proprietor: **JOHNSON MATTHEY PUBLIC LIMITED
COMPANY, 43 Hatton Garden, London, EC1N 8EE(GB)**

⑦② Inventor: **Jenkins, John Ward, Pink House Chalkhouse
Green, Near Reading Berkshire RG4 9AN(GB)**

⑦④ Representative: **Arthur, Bryan Edward et al, Withers &
Rogers 4 Dyer's Buildings Holborn, London
EC1N 2JT(GB)**

EP 0 217 532 B1

Note: Within nine months from the publication of the mention of the grant of the European patent, any person may give notice to the European Patent Office of opposition to the European patent granted. Notice of opposition shall be filed in a written reasoned statement. It shall not be deemed to have been filed until the opposition fee has been paid (Art. 99(1) European patent convention).

ACTORUM AG

Description

This invention relates to a catalytic hydrogen generator for use with methanol and oxygen (preferably supplied as air).

- 5 Existing catalytic hydrogen generators for use with methanol rely on the decomposition of methanol in the presence of water and copper chromite or zinc chromite in accordance with the following overall reaction:



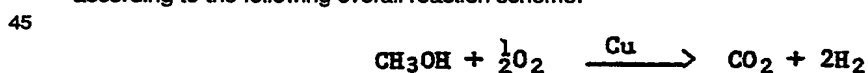
- The reaction only proceeds satisfactorily when the reaction zone is heated to above 300°C by externally generated heat which means that the reaction vessel must be provided with external heating means capable of generating large amounts of heat. The reaction is also performed at pressures of 20 to 30 bar which means that the reaction vessel must be pressure-resistant. In addition, existing generators produce significant quantities of carbon monoxide which is often an undesirable by-product. One of the objects of this invention is to minimise these disadvantages without causing complete oxidation of the methanol.

- 20 Accordingly this invention provides a catalytic hydrogen generator for use with mixtures of methanol and oxygen (preferably supplied as air) which generator contains a gas permeable catalyst system comprising

- a) an upstream zone into which the methanol and oxygen can be fed and which contains a catalyst comprising copper moieties supported on a refractory support and
 25 b) a downstream zone which can receive gases from the upstream zone and which contains a catalyst comprising copper moieties supported on a refractory support and mixed with a catalyst comprising moieties of one or more platinum group metals (hereinafter called "PG metals") chosen from platinum and palladium supported on a refractory support.

- 30 Preferably the refractory support comprises silica or a silicate especially when in the form of granules so that the mixture of copper and PG metal catalysts used in the downstream zone can be easily made by physically (for example tumble) mixing together granules supporting copper catalyst with granules supporting PG metal catalyst. Preferably the ratio of the volume of the support supporting the copper catalyst to the volume of the support supporting the PG metal catalyst is from 5 to 20:1.

- 35 The oxidation state of the copper and PG metal moieties is not known for certain and it probably varies during the generation of hydrogen. It has been found that when the mixture of methanol and oxygen is fed into the catalyst system at ambient temperature and pressure, the mixture initially permeates through the upstream zone without reacting and enters the downstream zone where the PG metal catalyst causes spontaneous oxidation of the methanol. The PG metal catalyst is not very selective towards the formation of hydrogen. However once the oxidation has started, the temperature in the downstream zone rises to that at which partial oxidation of methanol can be sustained in the upstream zone whereupon the front at which oxidation is occurring moves into the upstream zone and into the presence of the copper catalyst which is very selective to the production of hydrogen. It is believed that partial oxidation proceeds according to the following overall reaction scheme:



- 50 Yields of hydrogen as high as 80 to 90% of the theoretical maximum have been achieved which is a measure of the extent to which the catalyst system in the upstream zone is selective towards the production of hydrogen. Once started, this partial oxidation reaction generates enough heat to be self-sustaining and so no external heating means are needed. The partial oxidation reaction is also able to proceed at ambient pressure.

- 55 The catalyst system offers two further advantages. Firstly, soon after the oxidation of methanol has been initiated, the methanol oxidation reactions move away from the PG metal catalysts allowing the downstream zone to cool so minimising the losses of PG metal catalysts and the formation of carbon monoxide which would otherwise occur at high temperatures. Secondly, if any unreacted oxygen should arrive in the downstream zone, then it will be converted to water by the PG metal catalyst in the downstream zone so avoiding the possibility of dangerous amounts of oxygen being present in the hydrogen produced.

- 60 This invention also provides a process for the catalytic generation of hydrogen from a mixture of methanol and oxygen (preferably supplied as air) using a gas permeable catalyst system comprising:

- a) an upstream zone containing a catalyst comprising copper moieties supported on a refractory support and
 65 b) a downstream zone containing a catalyst comprising copper moieties supported on a refractory sup-

port and mixed with a catalyst comprising moieties of one or more metals chosen from platinum and palladium supported on a refractory support

wherein the mixture is fed into the upstream zone through which it permeates into the downstream zone where oxidation of methanol initiates spontaneously causing a rise in temperature to a temperature at which partial oxidation of methanol in the presence of a copper catalyst in the upstream zone can occur whereupon partial oxidation of methanol in the upstream zone commences and produces hydrogen. It is found that the partial oxidation reaction quickly establishes itself in a hot spot adjacent the place of entry of the mixture into the catalyst system. The precise size and location of this hot spot can be adjusted by varying the flow rate at which the mixture is fed into the system and it is preferred to adjust the flow rate so that the hot spot surrounds the place of entry of the mixture. The preferred flow rates are from 1 to 10 litres of gas mixture per hour per cm² of the cross-sectional area of the upstream zone in a plane transverse to the flow of the gases. Preferably the upstream and downstream zones are defined by a cylindrical reaction vessel having a length to diameter ratio of from 1 to 5:1. The temperature within the hot spot can be increased or decreased respectively by increasing or decreasing respectively the amount of oxygen supplied to the mixture. Preferably the ratio of the volume (at 18°C and 1 bar) of oxygen to the weight of methanol in the mixture is from 0.2 to 0.6:1 l/g. Preferably the catalyst system is provided with a combination of a thermocouple located within the hot spot and means responsive to the thermocouple for controlling the supply of oxygen to the mixture such that the combination can maintain the maximum temperature within the hot spot at or about a pre-determined level. The preferred maximum temperature lies in the range 300 to 600°C.

It is thought that the partial oxidation of methanol in the presence of a copper catalyst can occur at temperatures down to about 300°C. Accordingly the outer boundary of the hot spot is defined by the locus of points at which the temperature is 300°C. It appears that the presence of copper catalyst in a cooler zone downstream of the hot spot helps to minimise the production of carbon monoxide because at temperatures below 300°C, copper catalyses the carbon monoxide/steam shift reaction (i.e. $\text{CO} + \text{H}_2\text{O} \rightarrow \text{CO}_2 + \text{H}_2$) in a way which favours the production of carbon dioxide. Accordingly it is preferred that the volume of the hot spot should be no more than 50% of the volume of the upstream zone so as to ensure the presence of a cooler zone of adequate size.

The copper and PG metal moieties may be deposited on the refractory support by any conventional technique. The refractory support is preferably in the form of granules of diameter 1 to 5 mm so that the permeability of the catalyst system derives from the interstices between the granules.

It has been found that the tendency for carbon monoxide to be produced in temporary or localised incomplete partial oxidation reactions can be reduced by introducing steam into the mixture of methanol and oxygen preferably as soon as the hot spot has been established. Preferably the weight ratio of steam to methanol should be from 0.3 to 0.8 to 1.

The invention is further illustrated by the catalyst system described with reference to the drawing and by the following examples:

The drawing shows in section a catalyst system according to this invention.

The drawing shows a cylindrical reaction vessel 1 which houses a catalyst system composed of firstly an upstream zone 2 filled with granules 3 of a refractory support material which supports a copper catalyst and secondly a downstream zone 4 filled with a mixture of granules 5a and 5b of a refractory support material which in the case of granules 5a support a copper catalyst or in the case of granules 5b supports a PG metal catalyst. (For simplicity, only the top three layers of granules 3 or 5a and 5b are shown). Vessel 1 is provided with an inlet pipe 6 through which a mixture of methanol and air can be fed into upstream zone 2 and an outlet pipe 7 through which the gaseous products of the partial oxidation reaction can leave vessel 1.

When a mixture of methanol and air is fed into upstream zone 2, the mixture initially permeates through interstices 3a between granules 3 and enters downstream zone 4 where it contacts the PG metal catalyst and spontaneous oxidation of the methanol is initiated. The temperature rises to a temperature at which partial oxidation of methanol in the presence of a copper catalyst can occur whereupon partial oxidation commences in upstream zone 2 and quickly establishes itself within the boundary 8a of hot spot 8, which surrounds opening 9 of pipe 6 where the mixture enters the catalyst system.

Thermocouple 10 extends to the centre of hot spot 8 and is linked to a motorised valve 11 which controls the supply of air to pipe 6 and thence to hot spot 8. Valve 11 is responsive to thermocouple 10 in such a way that if the temperature at the centre of hot spot 8 exceeds a pre-determined value, valve 11 decreases the supply of air to hot spot 8 causing the temperature to fall. Alternatively if the temperature is too low, thermocouple 10 signals valve 11 to increase the supply of air.

Arrow 12 indicates the general direction of the flow of gases through upstream zone 2.

EXAMPLES 1 TO 5

A supported copper catalyst was made by wetting granules of silica with an aqueous solution of copper tetramine acetate and then washing and drying and heating the dried granules in air at 350°C to remove amine and acetate moieties. The granules had an average diameter of about 2 mm and the support-

ed catalyst produced contained 3 wt % of copper moieties based on the combined weight of the catalyst and support.

A supported palladium catalyst was made by wetting similar silica granules with an aqueous solution of palladium tetramine chloride and then washing, drying and heating the dried granules in air at 350°C to remove amine and chloride moieties. The supported catalyst produced contained 5 wt % of palladium moieties based on the combined weight of the catalyst and support.

Some of the granules supporting the copper catalyst were loaded into the upstream zone of a reaction vessel of the type shown in the drawing to produce the upstream zone of a catalyst system. The rest of the granules supporting the copper catalyst were tumble mixed with the granules supporting the palladium catalyst so as to produce a mixture in which the ratio of the volume of copper-supporting granules to the volume of palladium-supporting granules was 9:1. The mixture was then loaded into the downstream zone of a catalyst system. The vessel was cylindrical and was approximately 100 mm long and 40 mm in diameter. The lengths of the upstream and downstream zones were 80 mm and 20 mm respectively.

A mixture of methanol and air was fed into the upstream zone of the catalyst system. The mixture consisted of methanol fed at a rate of 10g/hour and air fed at one of various rates as specified in Table 1. The mixture permeated through the upstream zone into the downstream zone where it contacted the palladium catalyst and oxidation of the methanol initiated spontaneously. Within about 5 minutes of starting up, the temperature had risen to over 300°C and partial oxidation of methanol to produce hydrogen and carbon dioxide had commenced in the upstream zone. Within a further 10 minutes, the partial oxidation reaction was established within the boundary of an approximately spherical hot spot about 20 mm in diameter. The hot spot surrounded the point of entry of the mixture into the catalyst system. The maximum temperature in the hot spot, the proportions of methanol oxidised and the yields of hydrogen obtained at various feed rates for air are shown in Table 1. It will be seen that the yields of hydrogen are highest when the maximum temperature in the hot spot is above 300°C and in the range 450 to 500°C.

Table 1

Ex-ample	Air feed rate 1/hour	Ratio of air to methanol 1/g	Maximum temperature °C of hot spot	% Conversion of methanol	Yield of hydrogen 1/hour at 18°C and 1 bar	Yield as % of theoretical maximum
1	10	1	310	39	4.7	33
2	15	1.5	300	77	10.3	72
3	17.5	1.75	400	95	11.9	83
4	20	2	460	99	12.2	85
5	25	2.5	600	100	10.9	76

EXAMPLES 6 TO 10

The procedure of Examples 1 to 5 was repeated except that as soon as the hot spot had been established, 6g/hour of steam were injected into the mixture of methanol and air which was being fed to the upstream zone. It was found that the presence of the steam almost eliminated carbon dioxide production. The results obtained are shown in Table 2.

Table 2

Example	Air Feed Rate litres/hour	*Volume of carbon monoxide produced 1/hour steam added	*Volume of carbon monoxide produced 1/hour steam omitted
6	10	0	0
7	15	0	0.2
8	17.5	0	1.1
9	20	0	1.3
10	22.5	0.25	**

* Measured at 18°C and 1 bar

** 1.16 1/hour of carbon monoxide was obtained when the air feed rate was 25 1/hour.

Claims

1. A catalytic hydrogen generator for use with mixtures of methanol and oxygen which generator contains a gas permeable catalyst system comprising
 - 5 a) an upstream zone (2) into which the methanol and oxygen can be fed and which contains a catalyst comprising copper moieties supported on a refractory support (3) and
 - b) a downstream zone (4) which can receive gases from the upstream zone (2) and which contains a catalyst comprising copper moieties supported on a refractory support (5a) and mixed with a catalyst comprising moieties of one or more platinum group metals chosen from platinum and palladium supported on a refractory support (5b).
- 10 2. A hydrogen generator as claimed in Claim 1 comprising a downstream zone (4) in which the ratio of the volume of support (5a) supporting copper catalyst to the volume of support (5b) supporting palladium catalyst is from 5 to 20:1.
3. A hydrogen generator as claimed in Claim 1 wherein the catalyst in the downstream zone comprises palladium moieties.
- 15 4. A hydrogen generator as claimed in anyone of the preceding claims wherein the generator is provided with a combination of a thermocouple (10) located within the upstream zone (2) of the generator and means (11) responsive to the thermocouple (10) for controlling the supply oxygen to the mixture such that if the temperature sensed by the thermocouple (10) rises above or falls below a pre-determined value, the means (11) respectively decreases or increases the supply of oxygen to the mixture in response to a signal from the thermocouple (10).
- 20 5. A process for the catalytic generation of hydrogen from a mixture of methanol and oxygen using a gas permeable catalyst system comprising
 - a) an upstream zone (2) containing a catalyst comprising copper moieties supported on a refractory support (3) and
 - 25 b) a downstream zone (4) containing a catalyst comprising copper moieties supported on a refractory support (5a) and mixed with a catalyst comprising moieties of one or more metals chosen from platinum and palladium supported on a refractory support (5b).
 wherein the mixture is fed into the upstream zone (2) through which it permeates into the downstream zone (4) where oxidation of methanol initiates spontaneously causing a rise in temperature to a temperature at which partial oxidation of methanol in the presence of a copper catalyst in the upstream zone (2) can occur whereupon partial oxidation of methanol in the upstream zone (2) commences and produces hydrogen.
- 30 6. A process according to Claim 5 wherein steam is fed into the upstream zone (2) in addition to the mixture of methanol and oxygen.
7. A process according to Claim 5 or Claim 6 wherein the rate at which the mixture of methanol and oxygen is fed into the upstream zone (2) is adjusted so that partial oxidation of the methanol occurs in a hot spot (8) having a boundary (8a) defined by the locus of points having a temperature of 300°C and which hot spot surrounds (8) the place (9) where the mixture enters the upstream zone (2).
- 40 8. A process according to anyone of the preceding Claims wherein the ratio of the volume (at 18°C and 1 bar) of oxygen to the weight of methanol in the mixture is from 0.2 to 0.6:1 l/g.
9. A process according to Claim 7 wherein the rate at which the mixture of methanol and oxygen is fed into the upstream zone (2) and/or the ratio of oxygen to methanol in the mixture is adjusted to ensure that the volume of the hot spot (8) is no greater than 50% of the volume of the upstream zone (2).
- 45 10. A process according to any one of the preceding claims wherein the maximum temperature in the catalyst system is from 300 to 600°C.

Patentansprüche

- 50 1. Katalytischer Wasserstoff-Generator, bei dem Reaktionsgemische von Methanol und Sauerstoff zur Anwendung gelangen und der ein gasdurchlässiges Katalysatorsystem enthält, gekennzeichnet durch
 - 55 a) eine obere Reaktionszone (2), in welche Methanol und Sauerstoff eingespeist werden können und die einen auf einem feuerfesten Träger (3) getragenen Kupfer-Katalysator enthält, und
 - b) eine untere Reaktionszone (4), welche von der oberen Reaktionszone (2) Gase empfangen kann und die einen auf einem feuerfesten Träger (5a) getragenen Kupfer-Katalysator im Gemisch mit einem auf einem feuerfesten Träger (5b) getragenen Platinmetall-Katalysator mit ein oder mehr Platinmetallen, ausgewählt aus Platin und Palladium, enthält.
- 60 2. Wasserstoff-Generator nach Anspruch 1, dadurch gekennzeichnet, daß in der unteren Reaktionszone (4) das Verhältnis aus dem Volumen des Trägers (5a) für den Kupfer-Katalysator und dem Volumen des Trägers (5b) für den Platinmetall-Katalysator 5 bis 20 : 1 beträgt.
3. Wasserstoff-Generator nach Anspruch 1, dadurch gekennzeichnet, daß der in der unteren Reaktionszone (4) vorhandene Platinmetall-Katalysator Palladium enthält.
- 65 4. Wasserstoff-Generator nach einem der vorhergehenden Ansprüche, dadurch gekennzeichnet,

daß er eine Kombination aus einem in der oberen Reaktionszone (2) des Generators angeordnet n Thermoelement (10) und einem auf das Thermoelement (10) ansprechenden Strömungsregler (11) zur Steuerung der Zufuhr von Sauerstoff zum Reaktionsgemisch in einer Weise enthält, daß bei einem Anstieg oder Abfall der vom Thermoelement (10) gemessenen Temperatur auf über oder unter einen vorgegebenen Wert der Strömungsregler (11) die Zufuhr von Sauerstoff zum Reaktionsgemisch in Abhängigkeit von einem vom Thermoelement (10) empfangenen Signal entweder erniedrigt oder erhöht.

5. Verfahren zur katalytischen Erzeugung von Wasserstoff aus Gemischen von Methanol und Sauerstoff unter Verwendung eines gasdurchlässigen Katalysatorsystems, dadurch gekennzeichnet, daß in einen Wasserstoff-Generator, der

a) eine obere Reaktionszone (2), die einen auf einem feuerfesten Träger (3) getragenen Kupfer-Katalysator enthält, und

b) eine untere Reaktionszone (4), die einen auf einem feuerfesten Träger (5a) getragenen Kupfer-Katalysator mit einem auf einem feuerfesten Träger (5b) getragenen Platinmetall-Katalysator mit ein oder mehr Platinmetallen, ausgewählt aus Platin und Palladium, enthält,

ein Reaktionsgemisch von Methanol und Sauerstoff in die obere Reaktionszone (2) eingespeist wird und dieses Reaktionsgemisch nach Durchströmen der oberen Reaktionszone (2) dann in die untere Reaktionszone (4) geleitet wird, in welcher es durch eine spontane Einleitung der Oxidation des Methanols zu einem Anstieg der Temperatur auf eine Temperatur kommt, bei der eine teilweise Oxidation des Methanols in Anwesenheit des Kupfer-Katalysators in der oberen Reaktionszone (2) auftreten kann, worauf eine teilweise Oxidation des Methanols in der oberen Reaktionszone (2) beginnt und Wasserstoff gebildet wird.

6. Verfahren nach Anspruch 5, dadurch gekennzeichnet, daß in die obere Reaktionszone (2) zusätzlich zum Reaktionsgemisch von Methanol und Sauerstoff noch Wasserdampf eingeleitet wird.

7. Verfahren nach Anspruch 5 oder 6, dadurch gekennzeichnet, daß die Geschwindigkeit der Einspeisung des Reaktionsgemisches von Methanol und Sauerstoff in die obere Reaktionszone (2) so eingestellt wird, daß das Methanol an einer Heißzone (8) teilweise oxidiert wird, wobei diese Heißzone (8) eine Begrenzung (8a) aufweist, deren Ort durch Punkte mit einer Temperatur von 300°C definiert wird, und wobei die Heißzone (8) die Stelle (9) umgibt, an der das Reaktionsgemisch in die obere Reaktionszone (2) eintritt.

8. Verfahren nach einem der vorhergehenden Ansprüche, dadurch gekennzeichnet, daß das Verhältnis aus dem Volumen (bei 18°C und 1 bar) des Sauerstoffs und dem Gewicht des Methanols im Reaktionsgemisch 0,2 bis 0,6 : 1 l/g beträgt.

9. Verfahren nach Anspruch 7, dadurch gekennzeichnet, daß die Geschwindigkeit der Einspeisung des Reaktionsgemisches von Methanol und Sauerstoff in die obere Reaktionszone (2) und/oder das Verhältnis von Methanol und Sauerstoff im Reaktionsgemisch so eingestellt wird, daß das Volumen der Heißzone (8) nicht mehr als 50% des Volumens der oberen Reaktionszone (2) ausmacht.

10. Verfahren nach einem der vorhergehenden Ansprüche, dadurch gekennzeichnet, daß die maximale Temperatur im Katalysatorsystem 300 bis 600°C beträgt.

Revendications

1. Générateur d'hydrogène par catalyse, faisant appel à des mélanges de méthanol et d'oxygène, ce générateur contenant un système de catalyseurs perméables aux gaz, ce système comprenant

a) une zone-amont (2), dans laquelle on peut acheminer le méthanol et l'oxygène, cette zone contenant un catalyseur constitué de fragments de cuivre fixés sur un support réfractaire (3), et

b) une zone-aval (4), dans laquelle on peut introduire les gaz provenant de la zone-amont (2), cette zone-aval contenant un catalyseur constitué de fragments de cuivre fixés sur un support réfractaire (5a), ces fragments étant mélangés avec un catalyseur constitué de fragments d'un ou de plusieurs métaux du groupe du platine, choisis parmi le palladium et le platine, fixés sur un support réfractaire (5b).

2. Générateur d'hydrogène selon la revendication 1, comprenant une zone-aval (4) dans laquelle le rapport du volume du support (5a) sur lequel est fixé le catalyseur cuivre, au volume du support (5b) sur lequel est fixé le catalyseur palladium, est de 5 à 20 : 1.

3. Générateur d'hydrogène selon la revendication 1, dans lequel le catalyseur situé dans la zone-aval est constitué de fragments de palladium.

4. Générateur d'hydrogène selon l'une quelconque des revendications précédentes, dans lequel le générateur est muni d'une combinaison d'un thermocouple (10) situé au sein de la zone-amont (2) du générateur et d'un moyen (11) sensible au thermocouple (10), pour le réglage de l'apport en oxygène au mélange, de telle sorte que si la température perçue par le thermocouple (10) s'élève au-delà de ou s'abaisse en-dessous d'une valeur prédéterminée, le moyen (11) augmente ou diminue respectivement l'apport en oxygène au mélange, en réponse à un signal provenant du thermocouple (10).

5. Procédé pour la production catalytique d'hydrogène à partir d'un mélange de méthanol et d'oxygène, ce procédé faisant appel à un système de catalyseurs perméables aux gaz, ce système comprenant

a) une zone-amont (2) contenant un catalyseur constitué de fragments de cuivre fixés sur un support réfractaire (3), et

b) une zone-aval (4), contenant un catalyseur constitué de fragments de cuivre fixés sur un support réfractaire (5a), ces fragments étant mélangés avec un catalyseur constitué de fragments d'un ou de plusieurs métaux choisis parmi le palladium et le platine, fixés sur un support réfractaire (5b),

5 dans lequel le mélange est acheminé dans la zone-amont (2), à travers laquelle il passe pour pénétrer dans la zone-aval (4), où l'oxydation du méthanol se déclenche spontanément, provoquant ainsi une élévation de la température jusqu'à un degré tel que l'oxydation partielle du méthanol peut avoir lieu dans la zone-amont (2), en présence d'un catalyseur cuivre, à la suite de quoi, l'oxydation partielle du méthanol dans la zone-amont (2) débute et produit de l'hydrogène.

10 6. Procédé selon la revendication 5, dans lequel on achemine de la vapeur d'eau dans la zone-amont (2), en plus du mélange constitué de méthanol et d'oxygène.

15 7. Procédé selon la revendication 5 ou 6, dans lequel le débit auquel on achemine le mélange constitué de méthanol et d'oxygène dans la zone-amont (2) est réglé de telle sorte que l'oxydation partielle du méthanol ait lieu dans un point chaud (8) comportant une limite (8a) définie par le lieu des points où la température est de 300°C, ce point chaud (8) entourant l'endroit (9) par lequel le mélange entre dans la zone-amont (2).

20 8. Procédé selon l'une quelconque des revendications précédentes, dans lequel le rapport du volume (à 18°C et sous une pression de 1 bar) de l'oxygène au poids du méthanol dans le mélange est de 0,2 à 0,6 : 1 l/g.

25 9. Procédé selon la revendication 7, dans lequel le débit auquel on achemine le mélange constitué de méthanol et d'oxygène dans la zone-amont (2) et/ou le rapport de l'oxygène au méthanol dans le mélange est réglé pour garantir le fait que le volume du point chaud (8) ne dépasse pas 50% du volume de la zone-amont (2).

30 10. Procédé selon l'une quelconque des revendications précédentes, dans lequel la température maximale régnant dans le système de catalyseurs, est comprise dans l'intervalle allant de 300° à 600°C.

35

40

45

50

55

60

65

